

REMARKS

This Amendment provides a substitute specification; cancels claims 1-7, 9, 12, 14, and 15; and amends claims 8, 10, 11, 13, and 16-19. Support for the claim amendments is found, for example, in Fig. 1, in canceled claims 1-7, 9, and 12, and also in the specification at page 4, lines 6-7 and page 4, line 28 to page 5, line 7. Claims 8, 10, 11, 13, and 16-19 remain in this application.

Objection to the Specification

The specification was objected to for multiple spelling mistakes and format errors. As set forth above, Applicants enclose herewith a substitute specification correcting these spelling mistakes and format errors. The substitute specification contains no new matter. Approval of the substitute specification and reconsideration of the objection to the specification are respectfully requested.

Claim Objections

Claims 14 and 15 were objected to for improper dependency. As set forth above, Applicants have canceled claims 14 and 15, thereby rendering this objection moot.

Claims 2-13, and 16 were objected to for the informalities, grammatical errors, and spelling errors set forth on page 3 of the Office Action. As set forth above, Applicants have canceled claims 2-7, 9, and 12 and have amended the remaining claims to address and correct these errors. In view of the above amendments, reconsideration of these objections is respectfully requested.

Rejections Under 35 U.S.C. § 112, second paragraph

Claims 1-19 stand rejected for indefiniteness for the reasons set forth in paragraphs 4 and 5 of the Office Action. As set forth above, Applicants have corrected the improper antecedent basis language in the pending claims. Applicants have also deleted the terms “boundary line”, “hot section”, and “cold section”. Therefore, in view of the above amendments, reconsideration of these rejections is respectfully requested.

Rejections Under 35 U.S.C. § 102(b)

Claims 1-12, 16, and 17 stand rejected for anticipation by U.S. Patent No. 3,337,322 to Taylor. In view of the above amendments and the following remarks, reconsideration of these rejections is respectfully requested.

Claim 8, as amended, is directed to a method for making float glass with reduced defect density. The method comprises melting a glass composition to form a glass melt and pouring the glass melt in a float glass chamber. The float glass chamber comprises an upper plenum and a lower plenum, with a plurality of gas inlets and gas outlets in the upper plenum and lower plenum. The float glass chamber also includes a first chamber section and a second chamber section. The method includes controlling an atmosphere in the lower plenum of the first chamber section to have 0 to 3 volume percent hydrogen and controlling an atmosphere in the lower plenum of the second chamber section to have 0 to 10 volume percent hydrogen. The temperature of the glass melt in the first chamber section is higher than that in the second chamber section. A boundary between the first and second chamber sections is defined to be where a temperature of molten glass in the float glass chamber falls below a threshold temperature of at least 1600°F.

Taylor is directed to a method of making flat glass in which an atmosphere at the outlet of a float glass chamber consists of an inert gas having an admixture of 3% to 10% of a reducing gas. The atmosphere at the inlet consists of an inert gas having an admixture of 2% to 8% of a reducing gas. The head space over the bath between the inlet and the outlet has an atmosphere consisting of an inert gas with an admixture of 0.25% to 3% of a reducing gas. Taylor teaches that the reducing gas can be hydrogen (Taylor at column 2, line 59 to column 3, line 24 and column 4, line 27 to column 5, line 3).

In Taylor, the inlet and outlet regions are defined by walls 18 and 27, respectively, that physically divide the interior of the float chamber into the inlet, outlet, and intermediate regions. Taylor does not teach or suggest the method of amended claim 8 in which the float glass chamber comprises 2 sections, a first section and a second section, defined by a threshold temperature of the molten glass rather than a physical boundary. Nor does Taylor teach or suggest controlling the atmosphere in a lower plenum of these sections such that one section has an

atmosphere of 0 to 3 volume percent hydrogen and the other section has an atmosphere of 0 to 10 volume percent hydrogen. Therefore, claim 8, as amended, is not believed anticipated by Taylor. Reconsideration of the rejection of claim 8 is respectfully requested.

Claims 10, 11, 16, and 17 depend either directly or indirectly from, and add further limitations to, claim 8. Since these claims depend from a claim believed to be in condition for allowance, these claims are also believed to be in condition for allowance. Therefore, reconsideration of the rejections of these claims is respectfully requested.

Rejections Under 35 U.S.C. § 103(a)

Claims 13 and 19 stand rejected for obviousness over the teachings of Taylor in view of U.S. Patent No. 6,532,771 to Kobayashi et al. Claims 14 and 18 stand rejected for obviousness over the teachings of Taylor in view of U.S. Publication No. 2002/0059811 to Landa et al. Claim 15 stands rejected for obviousness over the teachings of Taylor and Landa in view of U.S. Patent No. 3,865,680 to Reese et al. In view of the above amendments and the following remarks, reconsideration of these rejections is respectfully requested.

Firstly, claims 14 and 15 have been canceled, thereby rendering these rejections moot.

Taylor has been discussed above. Kobayashi is directed to a method for controlling glass in an oxy-fuel furnace. Landa is directed to a method of making photochromic float glass. Reese is directed to an automobile windshield and a method of fabricating the windshield. However, none of the cited references, either alone or in combination, fairly teaches or suggests the invention as set forth in amended claim 8. Therefore, since remaining claims 13, 18, and 19 depend either directly or indirectly from claim 8, these claims are believed allowable for substantially the same reasons as discussed above with respect to claim 8. Reconsideration of the rejections of claims 13, 18, and 19 are respectfully requested.

Conclusion

In view of the above amendments and remarks, reconsideration of the objection to the specification and the rejections of claims 8, 10, 11, 13, and 16-19 are respectfully requested.

Respectfully submitted,

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Substitute Specification
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**Apparatus and Methods for Producing Float Glass
Having Reduced Defect Density**

Related Application

This application claims the benefits of United States Provisional Application Serial No. 60/414,516 filed September 27, 2002, which application is herein incorporated by reference in its entirety.

Field of the Invention

The present invention relates to a float glass chamber used to produce flat glass by the float glass process, and more specifically float glass chambers that can be used to yield glass having reduced defect density.

Background

The float glass process is well known for making sheets of glass. In a typical float glass process, batch materials are heated to form molten glass. The molten glass is then poured onto a bath of molten tin. The molten glass is drawn along the bath of molten tin and simultaneously cooled and attenuated to form a dimensionally stable continuous sheet of glass, typically referred to as a glass ribbon. The sheet is then removed from the bath for further processing.

Two types of furnaces are used in the float glass process, [] an air-fuel furnace and an oxy-fuel furnace. In an air-fuel furnace, fuel is mixed with warm air and combusted to provide heat to melt the glass batch materials.

In an oxy-fuel furnace, oxygen, not air, supports combustion. As a result, an oxy-fuel furnace provides a much more efficient melt than an air-fuel furnace because energy is no longer being wasted heating up nitrogen in the air and oxy-fuel flames have a higher flame temperature which that radiates more efficiently. The increased melting efficiency allows more tonnage to be processed through an oxy-fuel furnace than through a similarly sized [] air-fuel furnace.

Both air-fuel and oxy-fuel furnaces have water in their atmospheres. The head space (the area of the furnace above the molten glass) in an oxy-fuel furnace has a higher concentration of water than in an air-fuel furnace because the oxy-fuel atmosphere lacks the nitrogen provided in an air-fired fuel furnace that dilutes the total water formed by combustion. Stoichiometrically, the water typically constitutes about 66% by volume of the head space in an oxy-fuel furnace versus 18% in an air-fired fuel furnace. Since the amount of water in the glass melt is proportional to the square root of the concentration of water in the head space, glass melted in an oxy-fuel furnace has a 1-

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71.7 to 2 times higher water concentration than glass melted in a conventional air-fuel furnace. Typically, glass melted in an oxy-fuel furnace contains more than 0.045 weight percent water based on the total weight of the composition.

At the stage of the float glass process where molten glass is poured onto molten tin, the molten tin temperature in the float bath ranges from 1800°F to 1900°F (981°C to 1037°C). At 1800°F, at the glass-tin interface, water that diffuses out of the molten glass dissociates into hydrogen and oxygen. Because hydrogen isn't is not very soluble in tin at 1800°F, much of the hydrogen does not dissolve in the tin but remains in the atmosphere of the bath. Some of the hydrogen from the disassociation of water gets trapped at the interface between the molten glass and tin and ultimately impinges on the bottom surface of the glass ribbon and form defects along the ribbon surface typically referred to as open bottom bubbles. The open bottom bubbles can be described as voids in glass that generally have an inverted U-shape cross-section inverted U-shaped cross section. The presence of open bottom bubbles increases the overall defect density of the glass.

Customers set requirements for the defect density of glass for certain applications. The standards are very difficult to meet with conventional float glass processes due to the presence of open bottom bubbles.

The present invention provides a novel apparatus and method that yields float glass having a lower total defect density as a result of reduced open bottom bubble defects.

Summary of the Invention

a-In one embodiment, the present invention is a float glass chamber comprising: a hot section (first chamber section) having an atmosphere in at least the a lower plenum comprises comprising less than 3 percent hydrogen based on volume; and a cold section (second chamber section), wherein the boundary line between the hot section and the cold section is where the temperature of the glass falls below a threshold temperature.

In another embodiment, the present invention is a method for making float glass with reduced defect density comprising:

- a. melting a glass composition to form a glass melt; and
- b. pouring the glass melt in a float chamber having a hot section and an a cold section, the boundary line between the hot section and the cold section is where the temperature of the glass falls below a threshold temperature,

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wherein the hot section has an atmosphere in at least the a lower plenum comprises comprising less than 3 percent hydrogen based on volume.

Drawings

FIG. 1. is a sectional view of a float chamber according to the present invention, with portions removed for clarity.

Description of the Invention

As used herein, spatial or directional terms, such as "left", "right", "inner", "outer", "above", "below", "top", "bottom", and the like, relate to the invention as it is shown in the drawing figures. However, it is to be understood that the invention may assume various alternative orientations and, accordingly, such terms are not to be considered as limiting.

Unless otherwise indicated, all numbers expressing dimensions, physical characteristics, quantities of ingredients, reaction conditions and so forth, used in the specification and claims are to be understood as being modified in all instances by the term "about". Accordingly, unless indicated to the contrary, the numerical values set forth in the following specification and claims can vary depending upon the desired properties sought to be obtained by the present invention. At the very least, and not as an attempt to limit the application of the doctrine of equivalents to the scope of the claims, each numerical parameter should at least be construed in light of the number of reported significant digits and by applying ordinary rounding techniques. Moreover, all ranges disclosed herein are to be understood to encompass any and all subranges subsumed therein. For example, a stated range of "1 to 10" should be considered to include any and all subranges between (and inclusive of) the minimum value of 1 and the maximum value of 10; that is, all subranges beginning with a minimum value of 1 or more and ending with a maximum value of 10 or less, e.g., 5.5 to 10 or 3.2 to 7.8.

Conventional float glass processes are typically carried out using a float chamber as shown in FIG. 1. Non-limiting examples of float glass processes are disclosed in US Patent No. 3,083,551, US Patent No. 3,961,930, and US Patent No. 4,091,156, which are all hereby-herein incorporated by reference.

In a conventional float glass process, a glass batch composition is heated to a molten state and poured into the float chamber. Typically, the float chamber has a refractory roof 3 that divides the chamber into an upper plenum 1 and a lower plenum 2. The lower plenum contains the glass 4 and the tin 5. The upper plenum contains all of the overhead electrical heating elements to provide controlled heating of the liquid metal

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float bath and the formed glass ribbon. A controlled atmosphere is maintained in the chamber via gas inlets and outlets **6** and gas outlet(s) **7**.

The novel float glass chamber of the present invention comprises at least two sections[], a hot section and a cold section. The boundary line between the hot section and the cold section is where the temperature of the glass falls below a predetermined temperature, hereinafter referred to as the "threshold temperature," required for glass in the hot section. In a non-limiting embodiment of the present invention, there is no physical barrier between the hot section and the cold section.

In one non-limiting embodiment of the invention, the threshold temperature is 2100°F. In another non-limiting embodiment of the invention, the threshold temperature is 1800°F. In another non-limiting embodiment of the invention, the threshold temperature is 1600°F. The lower the threshold temperature for the hot section, the larger the hot section and the smaller the cold section and visa-vise versa.

In a non-limiting embodiment of the present invention, the hot section of the chamber is approximately 90 to 100 feet from the point where the molten glass is poured onto the tin. The cold section of the chamber is the next approximately 70 to 140 feet of chamber behind the hot section, depending on the size of the bath.

In a non-limiting embodiment of the present invention, numerous gas inlets and outlets are present in the upper plenum and lower plenum of the float chamber. Various gaseous mixtures can be pumped into the chamber through the gas inlets or out of the chamber through the gas outlets to control the atmosphere within the chamber.

In a non-limiting embodiment of the invention, the gas inlets to at least the lower plenum over the hot section of the chamber deliver in a gas comprising less than 1 weight percent hydrogen based on volume. The remainder of the gas can be an inert gas, such as but not limited to nitrogen. Under normal operating conditions, in one non-limiting embodiment of the present invention, the atmosphere of the lower plenum over the hot section of the chamber can comprise 3 percent hydrogen based on volume. In another non-limiting embodiment of the present invention, the atmosphere of the lower plenum over the hot section of the chamber can comprise 1 percent hydrogen based on volume.

Various mixtures of hydrogen and nitrogen or argon or ammonia in placed place of mixed gases can be pumped into the atmosphere of at least the lower plenum over the cold section of the chamber. In a non-limiting embodiment of the invention, the gaseous mixture can comprise up to 10 percent of the hydrogen based on volume. The rest of the gas can be nitrogen.

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The gas outlets in the float chamber can be used to remove gas from the chamber. In one non-limiting embodiment of the invention, up to 40 volume percent based on volume of the total flow of the gas pumped into the chamber as discussed above can be removed from the hot section. In this embodiment, it may be necessary to adjust the level of nitrogen in the atmosphere to prevent hydrogen from flowing upstream into the hot section of the chamber.

By reducing the hydrogen in the hot section of the float chamber, the present invention reduces the level of saturation of molten tin, specifically with respect to hydrogen, at the hot section of the float chamber. The molten tin is able to dissolve more hydrogen from the disassociation of water so open-bottom bubble defects in the glass are reduced.

The present invention also encompasses a method for producing glass. According to the present invention, glass can be produced via the following steps: adding glass batch materials to a furnace; melting the batch materials; pouring molten glass from the furnace into the float chamber; and removing the float glass from the float chamber.

The first step of the present invention comprises adding glass batch materials to a furnace. The furnace can be an air-fuel furnace or an oxy-fuel furnace. The glass batch materials can be of any conventional type including, but not limited to, conventional soda-lime-silica glass batch materials. A conventional glass composition can be characterized as follows:

from 65 to 75 weight percent SiO₂;
from 10 to 20 weight percent Na₂O;
from 5 to 15 weight percent CaO;
from 0 to 5 weight percent MgO;
from 0 to 5 weight percent Al₂O₃ ;
from 0 to 5 weight percent K₂O; and
from 0 to 2 weight percent Fe₂O₃.

All values are in weight percent based on the total weight of the glass composition.

The second step of the present invention comprises melting the batch materials in the furnace. The melting processes can be accomplished using techniques that are well known in the art. For example, in an oxy-fuel furnace, the batch materials can be melted by supplying oxygen and fuel to melt the batch materials.

The third step of the present invention involves pouring molten glass from the furnace into the float chamber. As is well known in the art, the molten glass flows onto the top of the molten tin and moves along the top of the tin from the hot section of the

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chamber to the cold section of the chamber. The temperature of the glass in the hot section and the cold section of the chamber are as discussed above. Also, the environments above the glass in the hot section and the cold section of the chamber are as discussed above.

The glass melt coming into the tin bath can contain water. The glass melt can have a water content equal to or greater than 0.045 weight percent based on the total weight percent of the composition.

The next step of the invention involves removing the float glass from the bath as is well known in the art.

After the float glass is removed from the float chamber, the glass is controllably cooled and cut into glass sheets. The sheet can be further processed, e.g. cut to shape and heat processed, to form a desired glass article.

The glass can also be coated. In a non-limiting embodiment of the invention, the glass is coated. The coating can include one or more coating layers and/or coating films. The coating can be of any desired type. For example, but not to be considered as limiting, the coating can be an electroconductive coating, a heatable coating, an antenna coating, or a solar control coating, such as a low emissivity coating. Non-limiting examples of solar control and antenna coatings are disclosed in U.S. Patent Nos. 4,898,789; 5,821,001; 4,716,086; 4,610,771; 4,902,580; 4,716,086; 4,806,220; 4,898,790; 4,834,857; 4,948,677; 5,059,295; and 5,028,579, which patents are herein incorporated by reference. Non-limiting examples of electroconductive coatings are disclosed in U.S. Patent Nos. 5,653,903 and 5,028,759, which are herein incorporated by reference.

Glass made by a float process typically ranges from a sheet thickness of 2 millimeter to 20 millimeters. Glass having the aforementioned thickness can be prepared on a conventional float line having a line speed ranging from 100 to 800 inches per minute. The required thickness of the glass is determined by the end use of the glass.

The present invention provides glass having reduced defect density^[,], specifically open-bottom bubbles. Such defects in the glass can be measured using on-line and off-line methods. An Automatic Inspection System manufactured by Inspection Technologies Inc. can be used to measure defects on-line. Defects can be measured off-line by visual inspection. The defect density of glass is measured as number of defects per 100 square feet. The standards for measuring defects in glass are well known in the art. For example, defects can be measured in categories from <0.06" to > 0.25".

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Glass produced according to the present invention can meet the various commercial standards for defect density. For example, car manufacturers set standards for defect density for automotive windshields. One automobile manufacturer requires automotive windshield glass production to have less than 1 total defect per 100 square feet.

The glass produced according to the present invention can be used as automotive transparencies, in colored glasses, laminated products, etc. as is well known in the art. A laminated product can comprise at least one piece of glass produced according to the present invention. Such a laminated product can be a windshield.

Examples

The invention is illustrated by the following non-limiting examples. The following is an example of a control run where hydrogen was in the lower plenum of the hot end and a run according to the present invention.

	Control	Example of the Invention
H ₂ in total chamber	1900 scfh	600 scfh
H ₂ in at least lower plenum of hot end	1300 scfh	0 scfh
Open Bottom Bubble defects	1.36 per 100 sq. ft.	0.07 per 100 sq. ft.
Thickness of glass	3 mm	3 mm
Tonnage	599 Tons per day	604 TPD
Threshold Temperature	1769°F	1761°F
H ₂ O in glass	0.049%	0.049%

Conclusion

The apparatus and method of the present invention allows float glass to be produced which has substantially reduced open bottom bubble defects as compared to conventional float glass.

The above examples are offered only to illustrate the present invention. The scope of the present invention is defined by the following claims.

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Abstract

A float glass chamber and related methods comprising a hot section having an atmosphere in at least the lower plenum comprises less than 3 percent hydrogen based on volume and a cold section, wherein the boundary line between the hot section and the cold section is where the temperature of the glass falls below a threshold temperature.